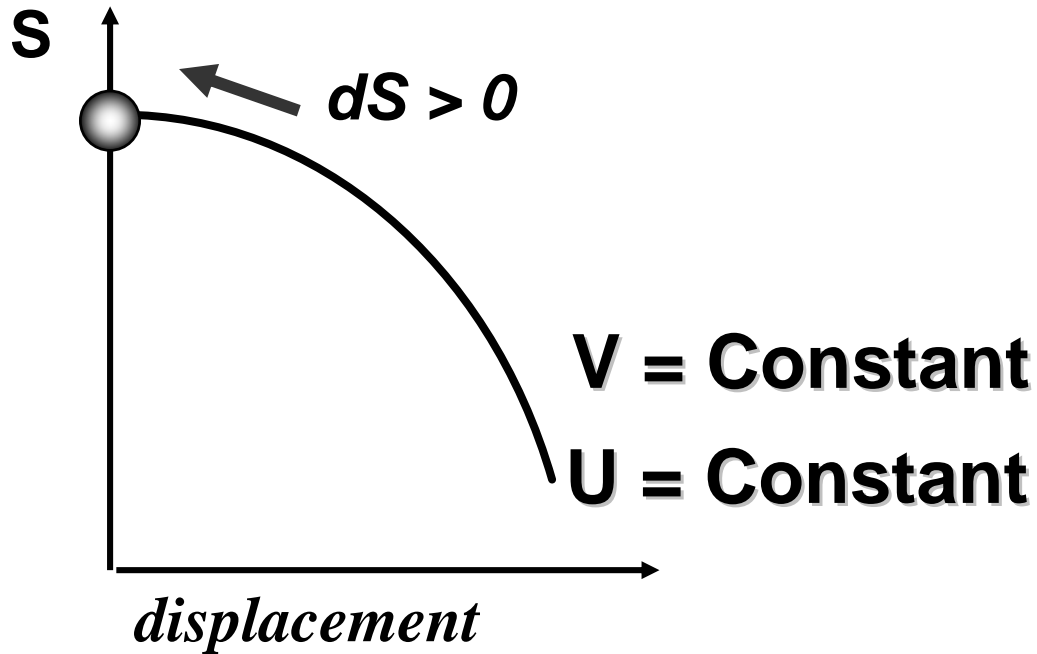


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# Chemical Equilibrium

# *The maximum entropy principle*

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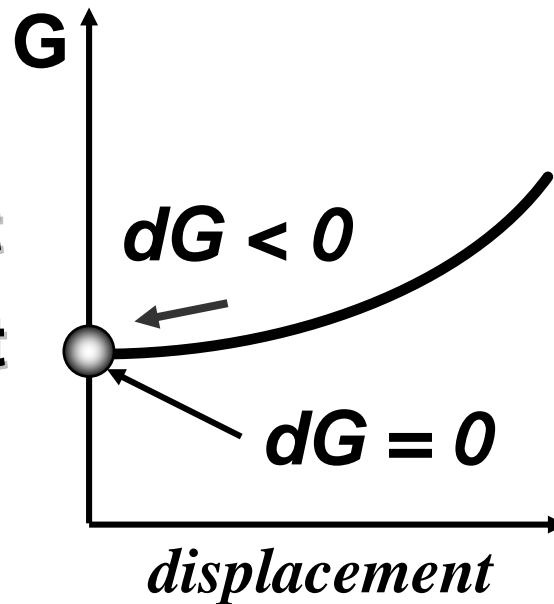
$$dS |_{U,V} \geq 0 \quad \text{For any spontaneous process}$$

# Gibbs function – Criterion for equilibrium

- Recall the Gibbs function

$$G = H - TS = U + PV - TS$$

**T = Constant**  
**P = Constant**



$$dG \Big|_{T,P} \leq 0$$

# *Chemical potential*

---

- For a multicomponent system, define the chemical potential of component  $i$ , symbolized by  $\mu_i$ , as:

$$\mu_i = \left( \frac{\partial G}{\partial n_i} \right)_{T, P, n_{j, j \neq i}}$$

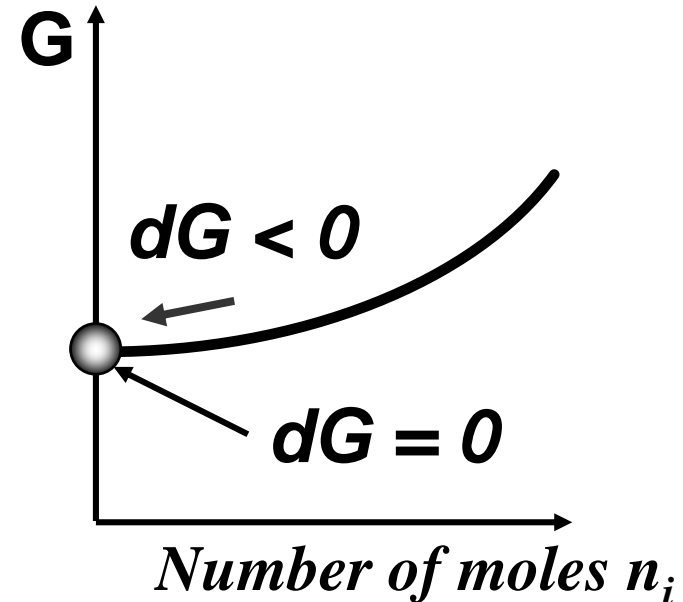
# Chemical potential

- The Gibbs function has been shown to be:

$$G = \sum_{i=1}^C n_i \mu_i$$

- And the condition for equilibrium takes the form:

$$dG \big|_{T,P} = \sum_{i=1}^C \mu_i dn_i = 0$$



# Single phase of a pure substance

- Let  $n$  be the number of moles
- Then  $G = n \mu$
- The chemical potential is then:

$$\mu = \frac{G}{n} = \bar{g}$$

# *Ideal gas mixture*

---

- The enthalpy and entropy of an ideal gas mixture are:

$$H = \sum_{i=1}^C n_i \bar{h}_i(T) \quad S = \sum_{i=1}^C n_i \bar{s}_i(T, p_i)$$

- $p_i = y_i p$  is the partial pressure of component  $i$  (the pressure that component  $i$  will have if it occupies the same volume as the mixture at the same temperature)

# The Gibbs function for a mixture of ideal gases

- For each gaseous species  $i$  that comprises an ideal gas mixture at constant  $T$  and constant  $P$ , we have:

$$\bar{g}_i = \bar{h}_i - T \bar{s}_i$$

- Associate a sub-volume  $v_i$  with each of the  $C$ -components:

$$T d\bar{s}_i = d\bar{u}_i + p d\bar{v}_i \quad \Rightarrow \quad d\bar{s}_i = \bar{c}_{v_i} \frac{dT}{T} + \bar{R} \frac{d\bar{v}_i}{\bar{v}_i}$$

# *The Gibbs function for a mixture of ideal gases*

---

$$d\bar{s}_i = \bar{c}_{v_i} \frac{dT}{T} + R \frac{d\bar{v}_i}{\bar{v}_i}$$

- The individual volumes  $\bar{v}_i$  are the 'internal degrees of freedom' which may adjust themselves so that the system attains equilibrium.
- An expression for the molar entropy can be calculated for any ideal gas species occupying volume  $\bar{v}_i$  at some temperature T by integrating that volume from some reference state.

# *The Gibbs function for a mixture of ideal gases*

---

$$d\bar{s}_i = \bar{c}_{v_i} \frac{dT}{T} + \bar{R} \frac{d\bar{v}_i}{\bar{v}_i}$$

- Introduce  $\bar{v}_i^{-ref}$  : the volume that a mole of isolated gas would occupy at some temperature T and some reference pressure  $P^{ref}$ .
- Integrate from  $\bar{v}_i^{-ref}$  to  $\bar{v}_i$  with constant T:

$$\bar{s}_i(\bar{v}_i) - \bar{s}_i(\bar{v}_i^{-ref}) = \bar{R} \ln \frac{\bar{v}_i}{\bar{v}_i^{-ref}}$$

# The Gibbs function for a mixture of ideal gases

$$\bar{s}_i(\bar{v}_i) - \bar{s}_i(\bar{v}_i^{\text{ref}}) = \bar{R} \ln \frac{\bar{v}_i}{\bar{v}_i^{\text{ref}}}$$

- Since for an ideal gas:

$$\frac{\bar{v}_i}{\bar{v}_i^{\text{ref}}} = \frac{p^{\text{ref}}}{p_i}$$

- We conclude:  $\bar{s}_i(\bar{v}_i) - \bar{s}_i(\bar{v}_i^{\text{ref}}) = \bar{R} \ln \frac{p^{\text{ref}}}{p_i} = \bar{R} \ln \frac{p^{\text{ref}}}{y_i p} =$

where, the partial pressure of component i is:

$$p_i = y_i p$$

# The Gibbs function for a mixture of ideal gases

$$\bar{s}_i(T, P) = \bar{s}_i^0(T) - \bar{R} \ln \frac{y_i P}{P_{ref}}$$

- Here  $p_i = y_i p$  is the partial pressure of component  $i$  – the pressure that the component  $i$  will have at temperature  $T$  occupying the mixture volume.

$$pV = n\bar{R}T, \quad p_i V = n_i \bar{R}T \Rightarrow \frac{p_i}{p} = \frac{n_i}{n} = y_i$$

# Ideal gas mixture

$$G = H - TS = \sum_{i=1}^C n_i \bar{h}_i(T) - T \sum_{i=1}^C n_i \bar{s}_i(T, p_i)$$
$$= \sum_{i=1}^C n_i (\bar{h}_i(T) - T \bar{s}_i(T, p_i))$$

- We introduce the molar Gibbs function of component  $i$  as:

$$\bar{g}_i(T, p_i) = \bar{h}_i(T) - T \bar{s}_i(T, p_i)$$

# Chemical potential of component $i$

$$\mu_i = \bar{g}_i(T, p_i) = \bar{h}_i(T) - T\bar{s}_i(T, p_i)$$

$$G = \sum_{i=1}^c n_i \bar{g}_i(T, p_i)$$

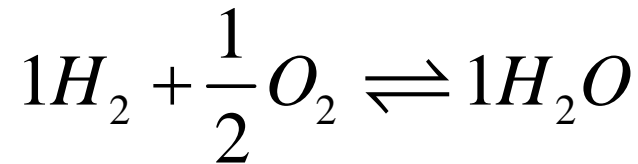
# Chemical potential of component i

$$\begin{aligned}\mu_i &= \bar{h}_i(T) - T \bar{s}_i(T, P) \\ &= \bar{h}_i(T) - T(\bar{s}_i^{-0}(T) - \bar{R} \ln \frac{y_i P}{P_{ref}}) \\ &= \bar{h}_i(T) - T \bar{s}_i^{-0}(T) + \bar{R} T \ln \frac{y_i P}{P_{ref}} \\ &= \bar{g}_i^{-0}(T) + \bar{R} T \ln \frac{y_i P}{P_{ref}} \text{ (ideal gas only)}\end{aligned}$$

# *Chemical equilibrium*

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- Consider a simple chemical reaction at equilibrium:

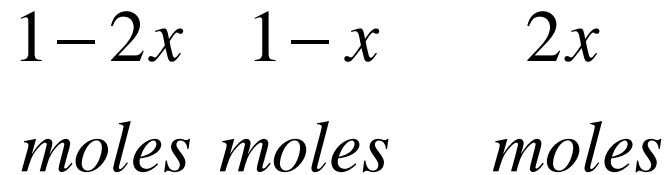
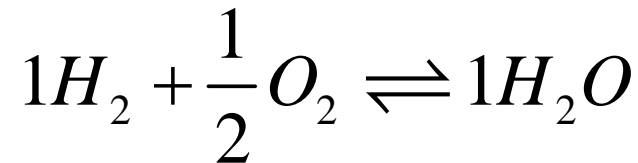


- Assume we have to start with 1 mole of H<sub>2</sub> and 1 mole of O<sub>2</sub>. Lets assume that 2x moles of H<sub>2</sub> react with x moles of O<sub>2</sub> giving us 2x moles of H<sub>2</sub>O. Thus at equilibrium, we have the following:
-

# Chemical equilibrium

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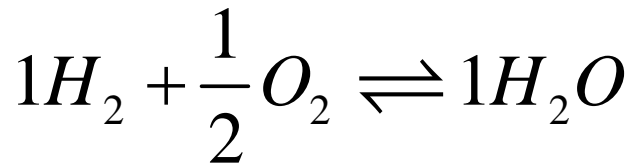
- At equilibrium:



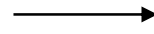
- Thus the mole fraction at equilibrium is:

$$1H_2 + \frac{1}{2}O_2 \rightleftharpoons 1H_2O$$
$$\begin{array}{ccc} \frac{1-2x}{2-x} & \frac{1-x}{2-x} & \frac{2x}{2-x} \end{array} \longrightarrow \begin{array}{ccc} dn_{H_2} = -dn_{H_2O}, & dn_{O_2} = -\frac{1}{2}dn_{H_2O} \\ \frac{-dn_{H_2}}{1} = \frac{-dn_{O_2}}{\frac{1}{2}} = \frac{dn_{H_2O}}{1} \end{array}$$

# Equation of reaction equilibrium

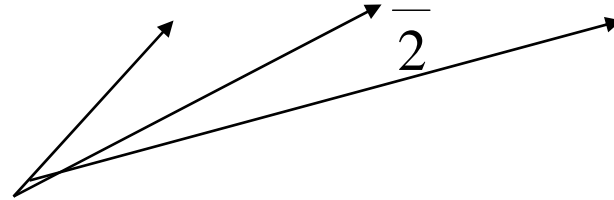


$$dn_{H_2} = -dn_{H_2O}, \quad dn_{O_2} = -\frac{1}{2}dn_{H_2O}$$



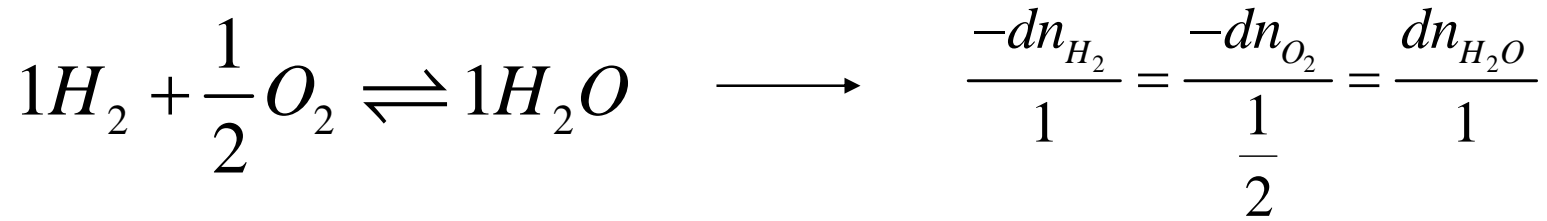
$$\frac{1-2x}{2-x} \quad \frac{1-x}{2-x} \quad \frac{2x}{2-x}$$

$$\frac{-dn_{H_2}}{1} = \frac{-dn_{O_2}}{\frac{1}{2}} = \frac{dn_{H_2O}}{1}$$



Stoichiometric  
coefficients

# Equation of reaction equilibrium



$$dG|_{T,P} = \mu_{H_2} dn_{H_2} + \mu_{O_2} dn_{O_2} + \mu_{H_2O} dn_{H_2O} \quad \Rightarrow$$

$$dG|_{T,P} = \left(-1\mu_{H_2} - \frac{1}{2}\mu_{O_2} + 1\mu_{H_2O}\right) dn_{H_2O}$$

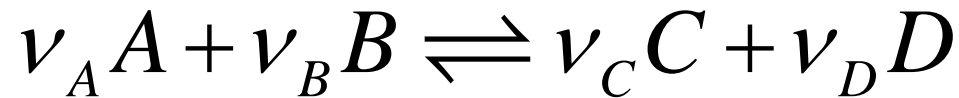
At equilibrium:  $dG|_{T,P} = 0$

$$-1\mu_{H_2} - \frac{1}{2}\mu_{O_2} + 1\mu_{H_2O} = 0$$

# *Consider a general reaction*

---

- For a reaction given by:



- The equation of reaction equilibrium is:

$$\nu_A \mu_A + \nu_B \mu_B = \nu_C \mu_C + \nu_D \mu_D$$

The composition that would be present at equilibrium for a given T and P can be determined by solving this equation. The solution procedure is simplified through the equilibrium constant concept introduced next.

# The equilibrium condition

Re-write the equilibrium condition in terms of the definition of  $g_i$ .

$$\nu_A \mu_A + \nu_B \mu_B = \nu_C \mu_C + \nu_D \mu_D$$

$$\nu_A \left( \bar{g}_A^{\ominus} + \bar{RT} \ln \frac{y_A P}{P_{ref}} \right) + \nu_B \left( \bar{g}_B^{\ominus} + \bar{RT} \ln \frac{y_B P}{P_{ref}} \right) =$$

$$\nu_C \left( \bar{g}_C^{\ominus} + \bar{RT} \ln \frac{y_C P}{P_{ref}} \right) + \nu_D \left( \bar{g}_D^{\ominus} + \bar{RT} \ln \frac{y_D P}{P_{ref}} \right)$$

$\bar{g}_i^{\ominus}$  all of these terms are at temperature T and 1 atm.

# *The equilibrium condition*

---

Rearrange terms to obtain:

$$v_A (\bar{g}_A^0 + \bar{RT} \ln \frac{y_A P}{P_{ref}}) + v_B (\bar{g}_B^0 + \bar{RT} \ln \frac{y_B P}{P_{ref}}) =$$

$$v_C (\bar{g}_C^0 + \bar{RT} \ln \frac{y_C P}{P_{ref}}) + v_D (\bar{g}_D^0 + \bar{RT} \ln \frac{y_D P}{P_{ref}})$$

↓

$$v_C \bar{g}_C^0 + v_D \bar{g}_D^0 - v_A \bar{g}_A^0 - v_B \bar{g}_B^0$$

$$= -\bar{RT} (v_C \ln \frac{y_C P}{P_{ref}} + v_D \ln \frac{y_D P}{P_{ref}} - v_A \ln \frac{y_A P}{P_{ref}} - v_B \ln \frac{y_B P}{P_{ref}})$$

# *The equilibrium condition*

---

Define:  $\Delta G^0 = \nu_C \bar{g}_C^0 + \nu_D \bar{g}_D^0 - \nu_A \bar{g}_A^0 - \nu_B \bar{g}_B^0$   
(computed at  $T$  and 1 atm)

$$\begin{aligned} -\frac{\Delta G^0}{RT} &= \nu_C \ln \frac{y_C P}{P_{ref}} + \nu_D \ln \frac{y_D P}{P_{ref}} - \nu_A \ln \frac{y_A P}{P_{ref}} - \nu_B \ln \frac{y_B P}{P_{ref}} = \\ &= \ln \left[ \frac{y_C^{\nu_C} y_D^{\nu_D}}{y_A^{\nu_A} y_B^{\nu_B}} \left( \frac{P}{P_{ref}} \right)^{\nu_C + \nu_D - \nu_A - \nu_B} \right] \end{aligned}$$

# *The equilibrium condition*

---

$$-\frac{\Delta G^0}{RT} = \ln \left[ \frac{y_C^{v_C} y_D^{v_D}}{y_A^{v_A} y_B^{v_B}} \left( \frac{P}{P_{ref}} \right)^{v_C + v_D - v_A - v_B} \right]$$

$$\downarrow$$
$$-\frac{\Delta G^0}{RT} = \ln K(T)$$

Where the equilibrium constant  $K(T)$  is defined as

$$K(T) = \frac{y_C^{v_C} y_D^{v_D}}{y_A^{v_A} y_B^{v_B}} \left( \frac{P}{P_{ref}} \right)^{v_C + v_D - v_A - v_B}$$

$\log_{10} K$  values over a range of temperatures is provided in Table A-27

# *Example*

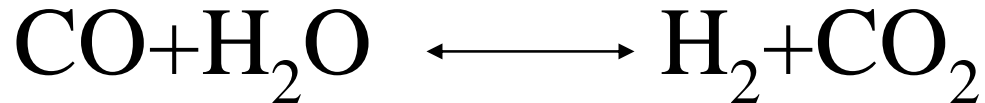
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Consider the gaseous reaction:  $P_4 \rightarrow 2P_2$ .  
For a system that has only gases  $P_4$  and  $P_2$  present, it is determined that at  $T = 1430\text{K}$  and  $P_{\text{total}} = 1 \text{ atm}$ , the mole fraction of  $P_4$  and  $P_2$  are equal ( $y_{P_4} = y_{P_2}$ ).  
Approximating the system as an ideal gas mixture, find the mole fractions of  $P_4$  at the same temperature ( $T = 1430\text{K}$ ) and at a total pressure  $P_{\text{total}} = 3/8 \text{ atm}$ .

# *Example*

---

- Consider the following gaseous reaction:

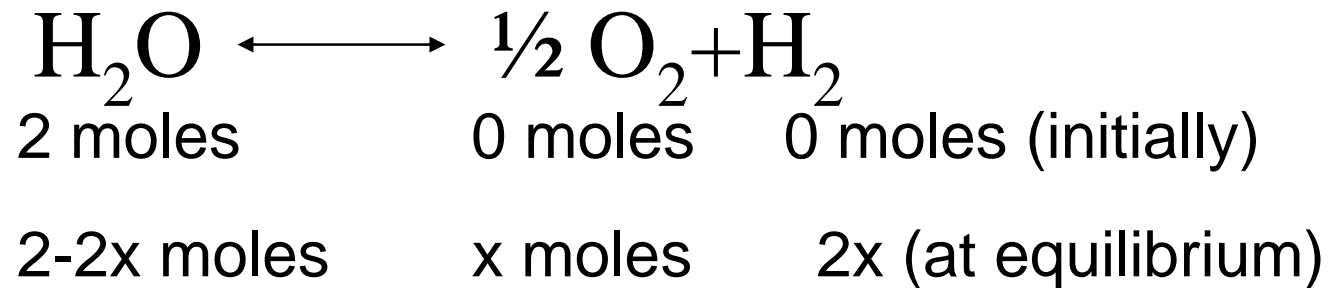
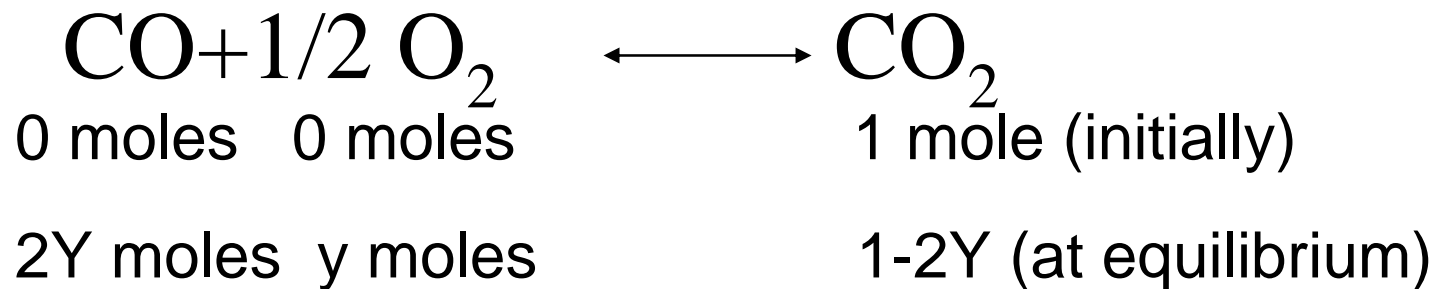
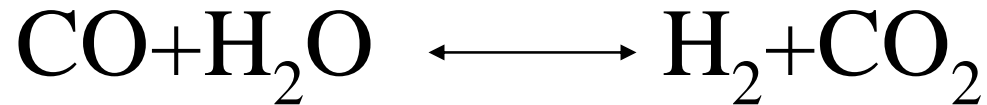


- Initially we have 2 moles of  $\text{H}_2\text{O}$  and 1 mole of  $\text{CO}_2$ .
- How many moles of oxygen exist at equilibrium?
- If the reaction is carried out at a different pressure, how will the concentration of  $\text{CO}$  vary?

# *Example*

---

- Write the reaction as a sum of 2 reactions!



# Example

- Note the mole fractions in the mixture

– CO:  $2y/(3+x+y)$

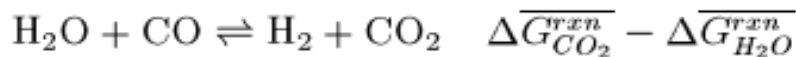
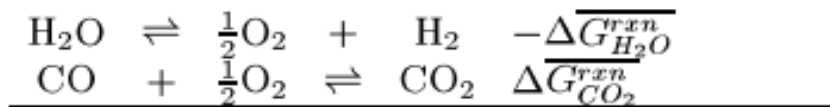
– CO<sub>2</sub>:  $(1-2y)/(3+x+y)$

– H<sub>2</sub>:  $2x/(3+x+y)$

– O<sub>2</sub>:  $(x+y)/(3+x+y)$

– H<sub>2</sub>O:  $(2-2x)/(3+x+y)$

Solve for x and y



$$\frac{\frac{1-2Y}{3+X+Y}}{\frac{2Y}{3+X+Y} \left(\frac{X+Y}{3+X+Y}\right)^{1/2}} = e^{-\left(\frac{\Delta\overline{G}_{\text{CO}_2}^{\text{rxn}}}{RT}\right)}$$

$$\frac{\frac{2X}{3+X+Y} \left(\frac{X+Y}{3+X+Y}\right)^{1/2}}{\frac{2-2X}{3+X+Y}} = e^{-\left(\frac{-\Delta\overline{G}_{\text{H}_2\text{O}}^{\text{rxn}}}{RT}\right)}$$